

Infrared Study of NO Adsorption and Reduction with C₃H₆ in the Presence of O₂ over CuO/Al₂O₃

Yawu Chi and Steven S. C. Chuang¹

Department of Chemical Engineering, The University of Akron, Akron, Ohio 44325-3906

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NO, NO/O₂, NO₂, and NO₂/O₂ adsorption on CuO/Al₂O₃ and selective catalytic reduction (SCR) of NO by C₃H₆ in the presence of 2% O₂ were investigated by infrared spectroscopy coupled with mass spectroscopy to provide insight into the mechanism of NO adsorption and reduction. Adsorption studies show that NO/O₂ adsorption at 298–723 K led to rapid formation of Cu²⁺<O>N and gradual formation of adsorbed (NO₃)₂; NO₂/O₂ adsorption led to immediate formation of (NO₃)₂ and gradual formation of Cu²⁺-O<O>N-O, Cu²⁺<O>N-O, and Cu²⁺<O>N; NO₂ adsorption alone did not produce (NO₃)₂. Temperature-programmed desorption shows that adsorbed (NO₃)₂ decomposed to N₂, N₂O, and NO at 644 K. Pulsing C₃H₆ into NO/O₂ over CuO/Al₂O₃ not only removed (NO₃)₂ but also reduced Cu²⁺ to Cu⁺/Cu⁰, resulting in the formation of N₂, N₂O, CO₂, and H₂O. Steady-state NO/O₂/C₃H₆ reaction on CuO/Al₂O₃ produced adsorbed C₃H₇-NO₂, CH₃COO⁻, Cu⁺-NCO, Cu⁰-CN, and Cu⁺-CO species, and N₂, CO₂, and H₂O as products. Dynamic behavior of adsorbates under transient conditions suggests that the steady-state SCR reaction may proceed via adsorbed C₃H₇-NO₂, Cu⁰-CN, and Cu⁺-NCO intermediates on Cu⁰/Cu⁺ surfaces. This study demonstrates that the pulse and steady-state SCR follows different reaction pathways toward N₂ and CO₂ products. © 2000

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Key Words: NO adsorption; nitrate formation; NO/O₂ adsorption; selective catalytic reduction; CuO/Al₂O₃; reaction mechanism; reaction intermediates; infrared spectroscopy; adsorbed nitrate.

INTRODUCTION

The development of an effective catalyst for NO decomposition and reduction in an oxidizing environment has been one of the most challenging tasks in environmental catalysis (1–21). Voluminous work has been done on catalyst screening and characterization to unravel the detrimental effect of oxygen in the NO decomposition to N₂ and O₂ (3–10). Addition of a reducing agent is required for the selective conversion of NO to N₂ in the presence of O₂ (3–5, 7, 8, 12–18).

¹ To whom correspondence should be addressed. E-mail: schuang@uakron.edu. Fax: (330) 972-5856.

CuO/Al₂O₃ was selected in the present study as a model catalyst for the NO adsorption and reduction studies for the following reasons: (i) the Cu surface state has been well characterized by examination of the infrared spectra of adsorbed CO and NO (22–25); (ii) Cu-exchanged ZSM-5 has been shown to be the most active NO decomposition catalyst; and (iii) Cu/Al₂O₃ has exhibited activity for NO reduction with CO and NH₃ (26, 27). Since the selective catalytic reduction (SCR) of NO_x is a redox reaction, a fundamental understanding of the Cu oxidation states and their adsorbates holds the key to the development of a NO decomposition and reduction mechanism and the determination of the limitation of CuO/Al₂O₃ for these reactions.

The objective of this study is to determine the structure and dynamic behavior of adsorbates as well as the oxidation states of adsorption sites for NO adsorption and reduction with C₃H₆ in the presence of O₂ over CuO/Al₂O₃. Infrared spectroscopy (IR) coupled with mass spectroscopy (MS) is used to determine the sequence of adsorbate and product formation for elucidation of reaction pathways and the nature of sites. The adsorbates observed in this study include Cu²⁺-O<O>N-O, Cu²⁺<O>N-O, Cu²⁺<O>N, and Cu²⁺(NO₃)₂ during the NO/O₂ adsorption as well as R-NO₂ (R = alkyl group), CH₃COO⁻, Cu⁺-NCO, Cu⁰-CN, and Cu⁺-CO species during the steady-state NO/O₂/C₃H₆ reaction. It has been reported that the SCR with hydrocarbons and/or NH₃ produced Cu²⁺-O<O>N-O, Cu²⁺<O>N-O, Cu²⁺<O>N, and Cu²⁺(NO₃)₂ on Cu/Al₂O₃ (13, 27, 29); R-NO₂ and/or R-ONO on Cu-Cr/Al₂O₃ (29), Pt/SiO₂ and Ce-ZSM-5 (3, 30, 31), Co-ZSM-5 (5, 32), Cu-ZSM-5 (33), and Na-H-mordenite (34); CH₃COO⁻ on Pt/Al₂O₃ (35) and Al₂O₃ (36); isocyanate (-NCO) on Cu/Al₂O₃ (28, 37), Cu-Cs/Al₂O₃ (38), Cu-ZSM-5 (13), Rh-Al-MCM-41 (39), and Pt/Al₂O₃ (35); and cyanide (-CN) species on Cu/Al₂O₃ (28), Pt/Al₂O₃ (35), Cu/ZrO₂ (40), and Co-ZSM-5 (41). The knowledge of adsorbate reactivities and their dynamic behavior may serve as a basis for the development of a comprehensive mechanism for the SCR of NO_x with hydrocarbons.

EXPERIMENTAL

Catalyst Precursor Preparation and Infrared (IR) Characterization

Copper nitrate/ γ - Al_2O_3 was prepared by impregnation of γ - Al_2O_3 (Alfa Products, SA = 100 m^2/g , pore size = 0.01–0.02 μm) with $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ (Strem Chemicals) solution. The sample, denoted as $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$, was dried overnight in air at 298 K. The Cu loading on the catalyst was 2.7 wt%. The amount of water was not determined. To obtain high resolution of infrared spectra for $\text{Cu}(\text{NO}_3)_2$, both $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ and $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ were mixed with KBr (Alfa Products, KBr spectrograde, ultra-pure) at a KBr/catalyst weight ratio of 10:1, and then were pressed into self-supporting disks for infrared characterization at 298 K. $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$, which was not mixed with KBr, was further characterized by IR spectroscopy coupled with temperature-programmed decomposition (TPDE) at a heating rate of 10 K/min from 298 to 773 K in a 75 cm^3/min He flow. The surface state of $\text{CuO}/\text{Al}_2\text{O}_3$ before and after NO/O_2 adsorption and SCR was characterized by IR spectroscopy with pulse CO chemisorption at 298 K.

Temperature-Programmed Desorption (TPD) of NO_x Adsorbates over $\text{CuO}/\text{Al}_2\text{O}_3$

The $\text{CuO}/\text{Al}_2\text{O}_3$ produced from temperature-programmed decomposition of $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ was used as the catalyst in this study. The $\text{CuO}/\text{Al}_2\text{O}_3$ was pretreated in a He flow at 773 K for 1 h and cooled to the desired temperature prior to each experiment. NO_x (i.e., NO, NO_2 , and NO_3^-) adsorbates on $\text{CuO}/\text{Al}_2\text{O}_3$ were produced by flowing various NO_x reactant gas mixtures (0.08% NO + 2% O_2 + 97.92% He; 1.06% NO_2 + 98.94% He; 0.08% NO_2 + 2% O_2 + 97.92% He) at 298, 523, 623, and 723 K. Gases used were 1.01% NO with He balance (AGA Specialty Gas), 99.99% O_2 (Praxair), 99.999% He (Praxair), C_3H_6 (LINDE Specialty Gas), and 99.994% CO (Praxair). Infrared analysis found less than 0.02% N_2O in the certified 1.01% NO. TPD of NO_x adsorbates on $\text{CuO}/\text{Al}_2\text{O}_3$ was performed from the adsorbing temperature (298 and 523 K) to 773 K at a heating rate of 10 K/min in a 75 cm^3/min He flow.

Pulsing C_3H_6 into the Steady-State NO/O_2 Flow and Steady-State SCR Reaction of $\text{NO}/\text{O}_2/\text{C}_3\text{H}_6$ over $\text{CuO}/\text{Al}_2\text{O}_3$

Upon both adsorbate and reactant/product concentrations reaching the steady state during a constant NO/O_2 flow, selective catalytic reduction (SCR) of NO was carried out by pulsing 1 cm^3 of C_3H_6 into the steady-state flow of NO and O_2 at 0.1 MPa and 523, 623, and 723 K. Three consecutive pulses of 1 cm^3 of C_3H_6 were used in the SCR of

NO to increase the NO conversion. Steady-state SCR reaction of 0.08% NO + 2% O_2 + 0.2% C_3H_6 + 97.72% He on $\text{CuO}/\text{Al}_2\text{O}_3$ was also conducted at a total flow rate of 75 cm^3/min , 0.1 MPa, and 523, 623, 673, 698, 723, and 773 K. The O_2 -to-NO ratio of 25 used in this study is in the lower region of the exhaust composition for lean burn combustion engines and power plants.

Infrared Spectroscopy, Mass Spectrometer, and X-Ray Diffraction (XRD) Analyses

Variation in adsorbate concentration was determined by using a Nicolet 55CX FTIR spectrometer at 4 cm^{-1} resolution. Infrared spectra were obtained by 32 coadded scans, which take 4 s for completion. Each coadded spectrum collected during TPD represents the average spectra of adsorbates during 1 K increases in temperature. Coadding a large number of scans increases the signal-to-noise ratio, but requires a longer sampling time, resulting in the loss of transient information. Hence, 32 coadded scans were used in the present study. Variation in reactant/product concentration was determined by using a Balzers QMG 112 and a Prisma QMS 200 mass spectrometer (MS) (Pfeiffer Vacuum Technology). The mass-to-charge ratios (m/e , i.e., amu) for MS monitoring were $m/e = 4$ for He, $m/e = 28$ for N_2 and CO, $m/e = 12$ (CO fragment) for separation of CO from $m/e = 28$, $m/e = 30$ for NO, $m/e = 32$ for O_2 , $m/e = 44$ for N_2O and CO_2 , $m/e = 22$ (CO_2 double ionization) for separation of CO_2 from $m/e = 44$, $m/e = 46$ for NO_2 , and $m/e = 41$ for C_3H_6 . The contribution of N_2O and NO_2 to $m/e = 30$ was determined by comparing the relative intensities of the fragment and parent ions of the calibrated N_2O , NO, and NO_2 pulse responses; the contribution of CO_2 to $m/e = 28$ was found to be negligible. The MS profiles of the reactants and products were obtained by multiplying their MS intensities by their calibration factors (42). The crystalline phases of $\text{CuO}/\text{Al}_2\text{O}_3$ were determined by using a Philips Analytical X-ray diffractometer with Cu $K\alpha$ radiation.

RESULTS

IR Spectra of $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ and $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$

Figure 1 compares the IR spectra of $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ and $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ at 298 K. The IR spectrum of $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ was obtained by subtracting the $\text{Al}_2\text{O}_3/\text{KBr}$ spectrum from the $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3/\text{KBr}$ spectrum; the IR spectrum of $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ was obtained by subtracting the KBr spectrum from the $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{KBr}$ spectrum. KBr has high IR transmission as shown in the inset. Bands below 1200 cm^{-1} for $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ were blocked by the Al_2O_3 support. Bands in the 1616–1636 cm^{-1} and 3400–3500 cm^{-1} regions are due to H_2O . $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ exhibited bands at 1767, 1385, and 823 cm^{-1} which is consistent with those reported

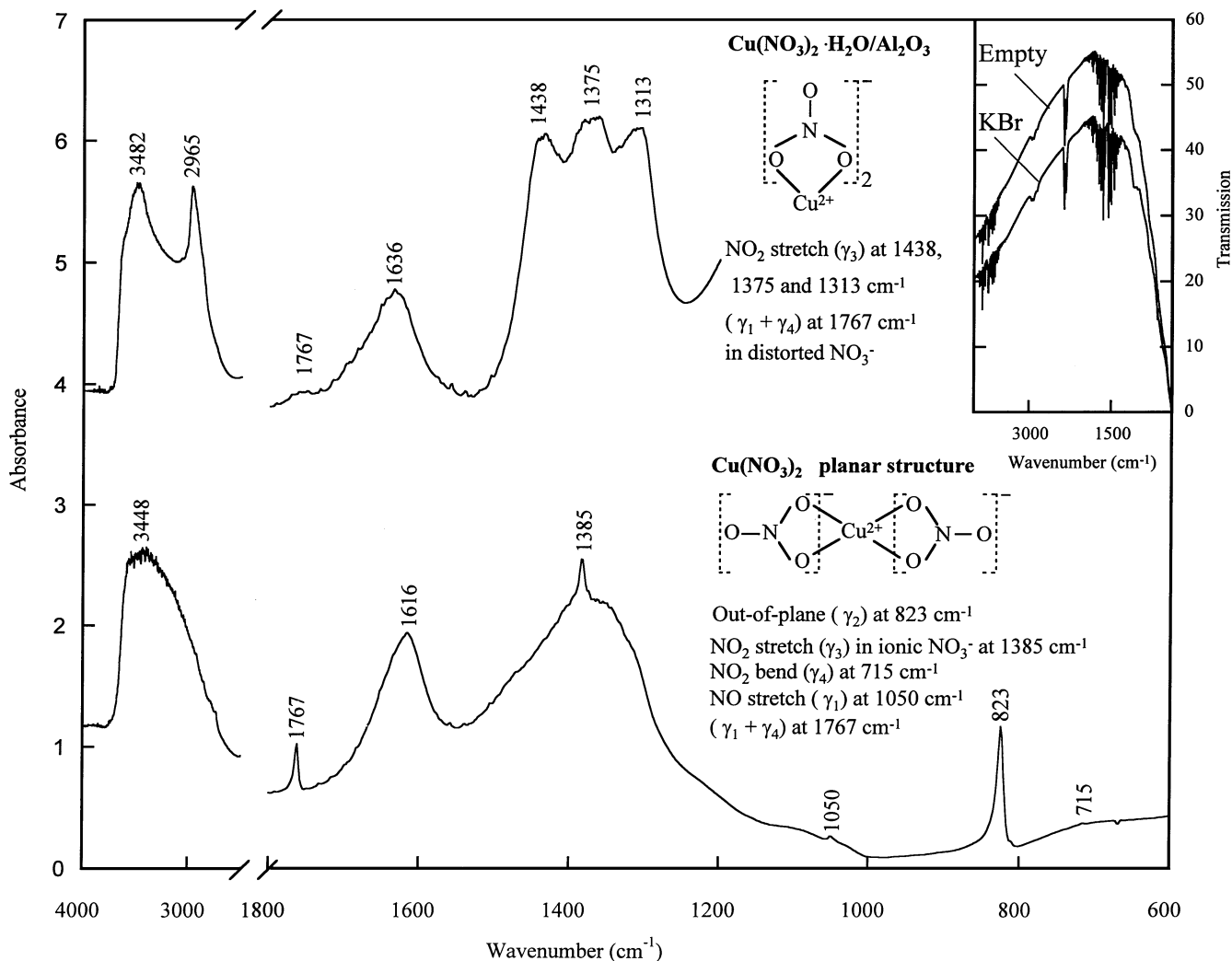


FIG. 1. IR spectra of Cu(NO₃)₂·H₂O/Al₂O₃ and Cu(NO₃)₂·3H₂O (infrared spectra of pure KBr as background and empty cell were inserted) at 298 K.

for Cu(NO₃)₂ (43–45). The band assignment is shown in Fig. 1. Cu(NO₃)₂·H₂O on Al₂O₃ exhibited a strong triplet in the 1313–1438 cm⁻¹ region, which may be due to the distortion from the D_{3h} of a NO₃⁻ species to the C_{2v} of a coordinated nitrato-ONO₂ species (43–45).

Temperature-Programmed Decomposition (TPDE) of Cu(NO₃)₂·H₂O/Al₂O₃

Figure 2 shows the normalized MS intensity product profiles and *in situ* IR spectra taken during the temperature-programmed decomposition (TPDE) of Cu(NO₃)₂·H₂O/Al₂O₃. Absorbance spectra of Cu(NO₃)₂·H₂O/Al₂O₃ during TPDE were obtained by ratioing the transmission spectra of Cu(NO₃)₂·H₂O/Al₂O₃ to that of CuO/Al₂O₃ at the specific temperature. CuO/Al₂O₃ transmission spectra, which were reserved as background spectra, were collected while the reactor cooled from 773 to 298 K in a He flow

after TPDE. Cu(NO₃)₂·H₂O exhibited a broad band in the 1305–1442 cm⁻¹ region, in contrast to the clear triplet bands observed for Cu(NO₃)₂·H₂O/Al₂O₃ mixed with KBr in Fig. 1. Dilution of Cu(NO₃)₂·H₂O/Al₂O₃ with KBr in Fig. 1 increased the resolution of the triplet bands due to distorted [NO₃⁻]₂. To avoid the complication from NO adsorption on KBr, Cu(NO₃)₂·H₂O/Al₂O₃ and CuO/Al₂O₃ resulting from Cu(NO₃)₂·H₂O/Al₂O₃ TPDE were not mixed with KBr during TPD and reaction studies. Cu(NO₃)₂·H₂O/Al₂O₃ began to decompose at 360 K, releasing H₂O, NO, N₂O, N₂, O₂, and NO₂. The MS intensity profiles were normalized with the calibration factors of each species so that the shaded area under the MS profiles corresponded to the product amount in micromoles. Evolution of adsorbed H₂O corresponds to the gradual decrease of the water band at 1620–1667 cm⁻¹. The peak temperature for the H₂O MS profile at 465 K is lower than those for NO, N₂O, and N₂ (at 485 K). The formation of these gaseous

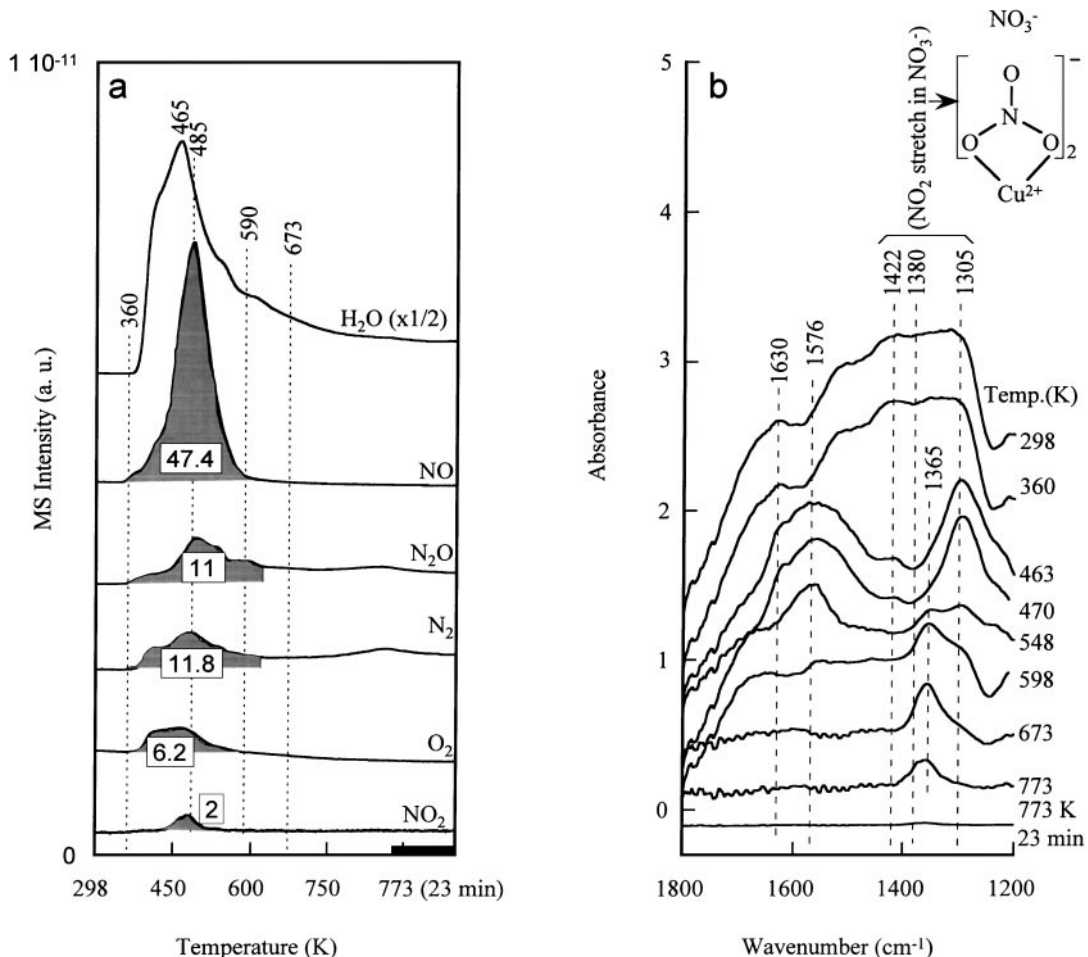


FIG. 2. (a) Normalized product MS profiles and (b) *in situ* IR spectra taken during the $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ decomposition from 298 to 773 K at a heating rate of 10 K/min. (H_2O MS profile was decreased by multiplying by $\frac{1}{2}$.)

species corresponding to a significant drop in the distorted $[\text{NO}_3^-]_2$ intensity indicates the decomposition of $\text{Cu}(\text{NO}_3)_2$ on Al_2O_3 to NO, N_2O , N_2 , O_2 , and NO_2 . The amount of decomposed product is indicated in micromoles in Fig. 2a, giving a N/O ratio of 1.3 and a NO/ O_2 ratio of 7.8. It is indeed surprising to observe the formation of a significant amount of N_2 and O_2 . Increasing the temperature to 673 K produced a well-defined band at 1365 cm^{-1} with a shift to 1370 cm^{-1} at 773 K.

No direct information is available to distinguish the difference between the species giving broad bands at 1422, 1380, and 1305 cm^{-1} and the adsorbed species giving the single band at $1365\text{--}1370 \text{ cm}^{-1}$. We tentatively assign the singly symmetric band at $1365\text{--}1380 \text{ cm}^{-1}$ to $(\text{NO}_3^-)_2$ since it resembles in some aspects that of $\text{Cu}^{2+}(\text{NO}_3^-)_2$. The appearance of this feature at temperatures above 548 K suggests that it is formed from the decomposition product of $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$. To distinguish the difference between the singly symmetric band at $1365\text{--}1390 \text{ cm}^{-1}$ and the broad triplet bands in the same region, we denote the

former as $(\text{NO}_3^-)_2$, the undistorted structure, and the latter as $[\text{NO}_3^-]_2$, the distorted structure.

X-ray diffraction (XRD) of the decomposed $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ gave only the $\gamma\text{-Al}_2\text{O}_3$ pattern (not shown). No XRD pattern for CuO or CuO_x was observed, suggesting that $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ decomposed to highly dispersed Cu oxide (46). The decomposed $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$, denoted as $\text{CuO}/\text{Al}_2\text{O}_3$, was used as a catalyst for the NO decomposition and reduction studies. Further characterization of the $\text{CuO}/\text{Al}_2\text{O}_3$ surface state by IR studies of CO adsorption will be presented and discussed later.

TPD of Adsorbates on $\text{CuO}/\text{Al}_2\text{O}_3$ from 298/523 to 773 K

Figure 3 shows the normalized product MS intensity profiles and *in situ* IR spectra of adsorbed NO_x species on $\text{CuO}/\text{Al}_2\text{O}_3$ taken during TPD from 298 to 773 K. Figure 3b shows that exposure of $\text{CuO}/\text{Al}_2\text{O}_3$ to a 0.08% $\text{NO} + 2\% \text{O}_2 + 97.92\% \text{He}$ flow at 298 K produced bands

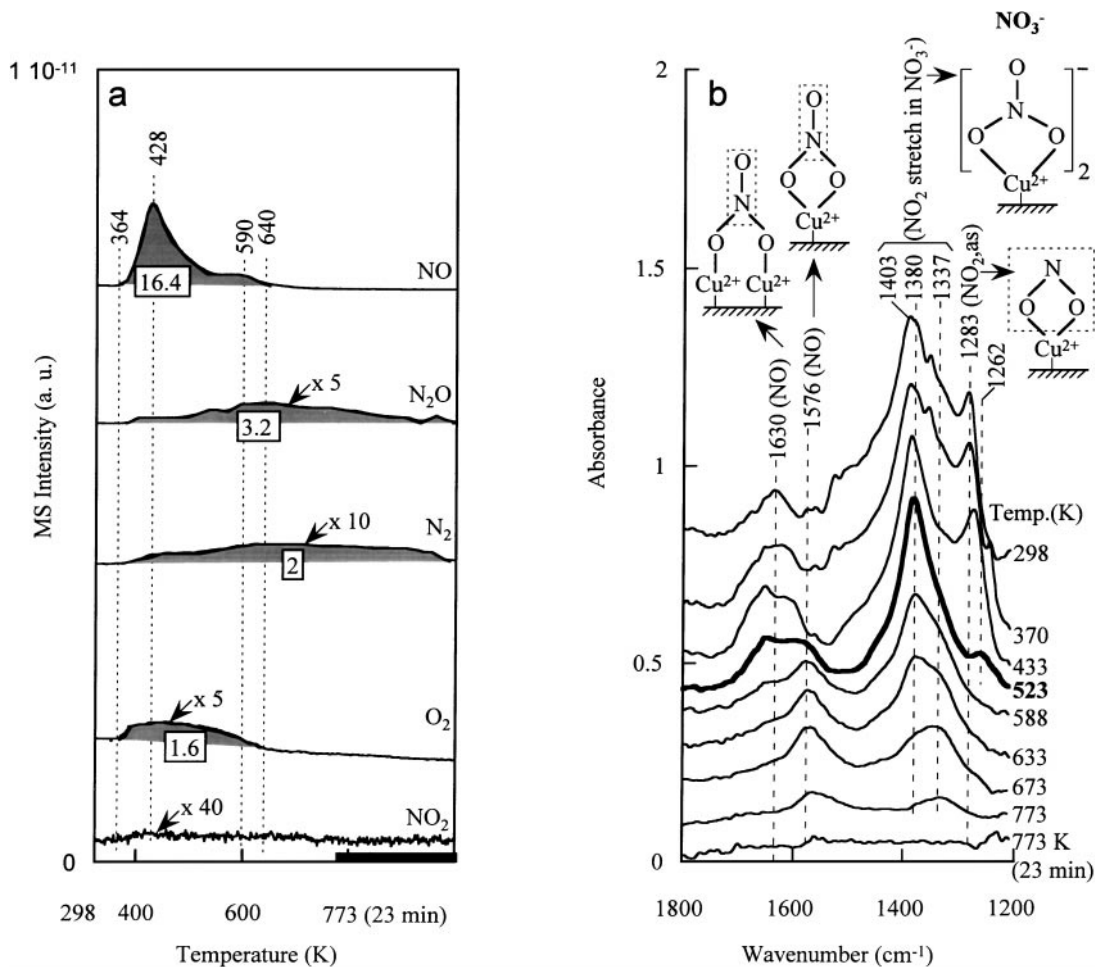


FIG. 3. (a) Normalized product MS profiles and (b) *in situ* IR spectra taken during the TPD of adsorbates (produced from flow of 0.08% NO + 2% O₂ + 97.92% He at 298 K) over CuO/Al₂O₃ from 298 to 773 K at a heating rate of 10 K/min. (N₂O, N₂, O₂, and NO₂ MS profiles were enlarged by multiplying by 5, 10, 5, and 40, respectively.)

at 1403, 1380, and 1337 cm⁻¹, bridging bidentate nitrate (Cu²⁺-O>N-O) at 1630 cm⁻¹, chelating bidentate nitrate (Cu²⁺<O>N-O) at 1576 cm⁻¹, and the overlapping component of their NO₂ asymmetric vibration with chelating nitro (Cu²⁺<O>N) at 1283 cm⁻¹ (15, 16, 47–52). These adsorbates may be associated with Cu²⁺ sites as observed in the CO adsorption studies discussed in the latter part of this study, which showed that the CuO/Al₂O₃ exposed to NO/O₂ contained Cu²⁺ sites. It should be noted that the notation used for these adsorbed NO_x species did not include the charge balance. The charge on Cu²⁺ is expected to be balanced by the surface oxygen anion and adsorbed nitrate/nitro species. The bands at 1403, 1380, and 1337 cm⁻¹ resembled those observed on Cu(NO₃)₂·H₂O/Al₂O₃, and can be assigned to the NO₂ stretch of a distorted [NO₃⁻]₂ adsorbed on Cu²⁺.

The distorted [NO₃⁻]₂ adsorbed on CuO/Al₂O₃ began decomposing at 364 K, releasing NO, N₂O, N₂, and O₂ (Fig. 3). The amount (micromoles) of products released, equivalent to the area under the product profile, is also

indicated Fig. 3a. Evolution of NO and O₂, the primary products in the 364–640 K region, corresponds to the gradual decrease in the IR intensities of Cu²⁺-O>N-O at 1630 cm⁻¹, [NO₃⁻]₂ at 1380 cm⁻¹, and Cu²⁺<O>N at 1262–1278 cm⁻¹. Increasing the temperature to 523 K caused the broad distorted [NO₃⁻]₂ band to sharpen. Increasing the temperature to 588 K produced Cu²⁺<O>N-O at 1576 cm⁻¹. Cu²⁺<O>N-O, also observed during Cu(NO₃)₂/Al₂O₃ decomposition in the 463–548 K region in Fig. 2b, could be produced from the readsorption of NO and O₂. In fact, NO/O₂ adsorption on CuO/Al₂O₃ at 523 K confirmed the formation of dominant Cu²⁺<O>N-O. A further increase in temperature from 588 to 773 K caused the (NO₃⁻)₂ to shift from 1380 to 1337 cm⁻¹. Evolution of N₂O and a small fraction of N₂ at temperatures above 673 K corresponded to decreases in the IR intensities of both Cu²⁺<O>N-O at 1576 cm⁻¹ and [NO₃⁻]₂ at 1337 cm⁻¹. Comparison of the MS profiles in Fig. 3a with those in Fig. 2a shows that NO and O₂ desorption exhibited similar profiles. The major difference is that N₂O and N₂

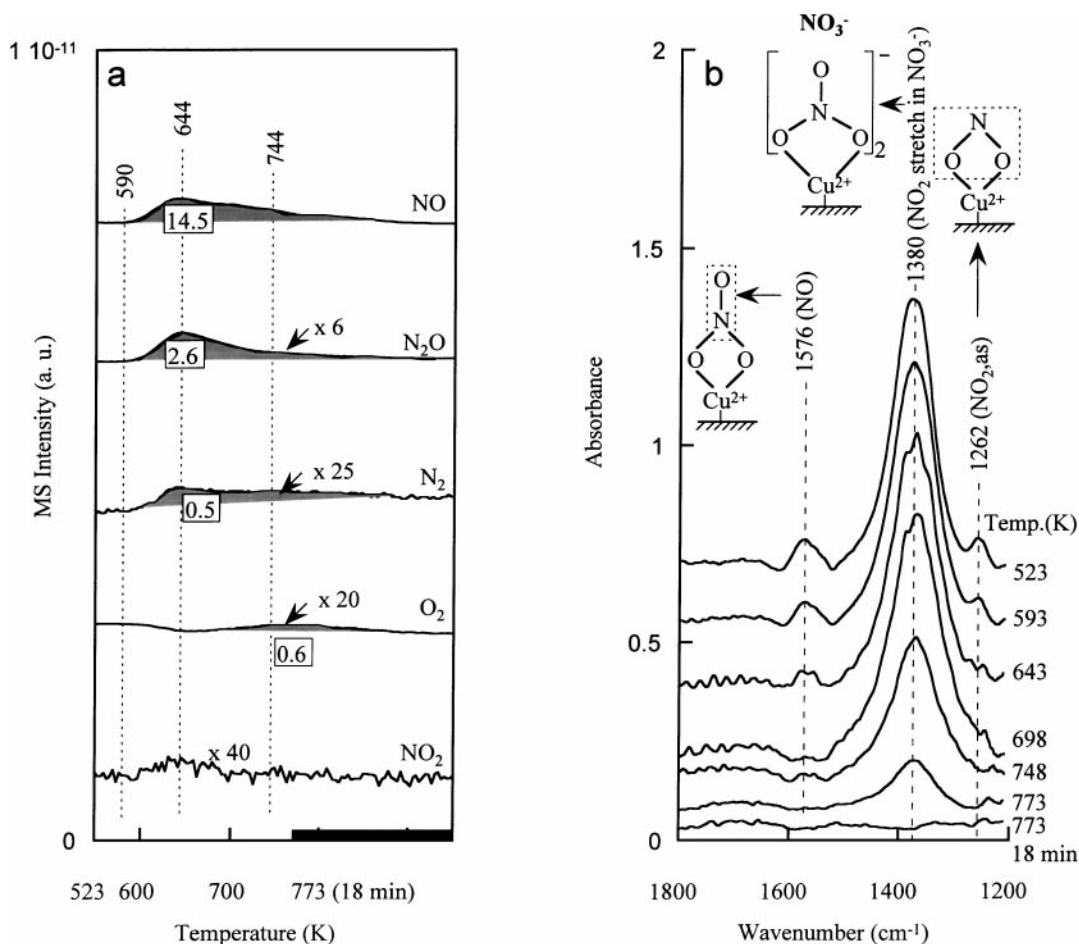


FIG. 4. (a) Normalized product MS profiles and (b) *in situ* IR spectra taken during the TPD of adsorbates (produced from flow of 0.08% NO + 2% O₂ + 97.92% He at 523 K) over CuO/Al₂O₃ from 523 to 773 K at a heating rate of 10 K/min. (N₂O, N₂, O₂, and NO₂ MS profiles were enlarged by multiplying by 6, 25, 20, and 40, respectively.)

profiles lagged behind those of NO and O₂ with the presence of Cu²⁺<O>N-O in the 588–773 K region in Fig. 3a.

Figure 4 shows the normalized product MS intensity profiles and *in situ* IR spectra of adsorbed NO_x species on CuO/Al₂O₃ taken during TPD from 523 to 773 K. Adsorbed (NO₃⁻)₂ at 1380 cm⁻¹, Cu²⁺<O>N-O at 1576 cm⁻¹, and Cu²⁺<O>N at 1262 cm⁻¹ produced from NO/O₂ adsorption at 523 K began to decompose at 590 K, releasing NO, N₂O, and N₂ with peak intensities at 644 K. Comparison of product MS profiles and IR spectra of adsorbates in Fig. 4 to those in Fig. 3 suggests that desorption/decomposition of distorted [NO₃⁻]₂, Cu²⁺<O>N-O, and Cu²⁺<O>N were responsible for O₂ and part of the NO formation at 428 K, while (NO₃⁻)₂ at 1380 cm⁻¹ and Cu²⁺<O>N-O were mainly responsible for the NO, N₂O, and N₂ formation at around 644 K.

Adsorption of NO and O₂ on CuO/Al₂O₃

Figure 5 shows *in situ* IR spectra produced from the coadsorption of 0.08% NO and 2% O₂ at 298, 523, and 623 K as

well as 0.08% NO adsorption followed by 2% O₂ at 523 K on CuO/Al₂O₃. Flowing 0.08% NO/2% O₂ over CuO/Al₂O₃ at 298 K produced the chelating nitro Cu²⁺<O>N at 1262 cm⁻¹, Cu²⁺<O>N-O at 1620 cm⁻¹, and adsorbed NO^{δ-} at 1836 cm⁻¹. Prolonged exposure to NO/O₂ produced Cu²⁺<O>N-O at 1576 and 1283 cm⁻¹ and the (NO₃⁻)₂ band at 1380 cm⁻¹ in addition to nitro and bridging bidentate nitrate (15, 16, 47–52). Flowing 0.08% NO/2% O₂ at 523 K produced the same adsorbates as those produced at 298 K, but at a higher formation rate than that at 298 K. The overlapping of Cu²⁺<O>N at 1251 cm⁻¹ with Cu²⁺<O>N-O at 1262 cm⁻¹ results in the formation of a prominent band at 1262 cm⁻¹. The significant fraction of 1262 cm⁻¹ is due to the NO₂ asymmetric vibration of Cu²⁺<O>N rather than that of Cu²⁺<O>N-O since Cu²⁺<O>N-O gives a lower intensity at 1262 cm⁻¹ than at 1570 cm⁻¹. The amount of adsorbed NO determined by the NO MS profile (not shown) is 0.50 mol per mole of Cu²⁺ at 523 K.

Exposure of CuO/Al₂O₃ to 0.08% NO at 523 K produced Cu²⁺<O>N-O at 1570 and 1233 cm⁻¹, nitrito (Cu²⁺-O-N=O) at 1315 cm⁻¹, and chelating nitro Cu²⁺<O>N at

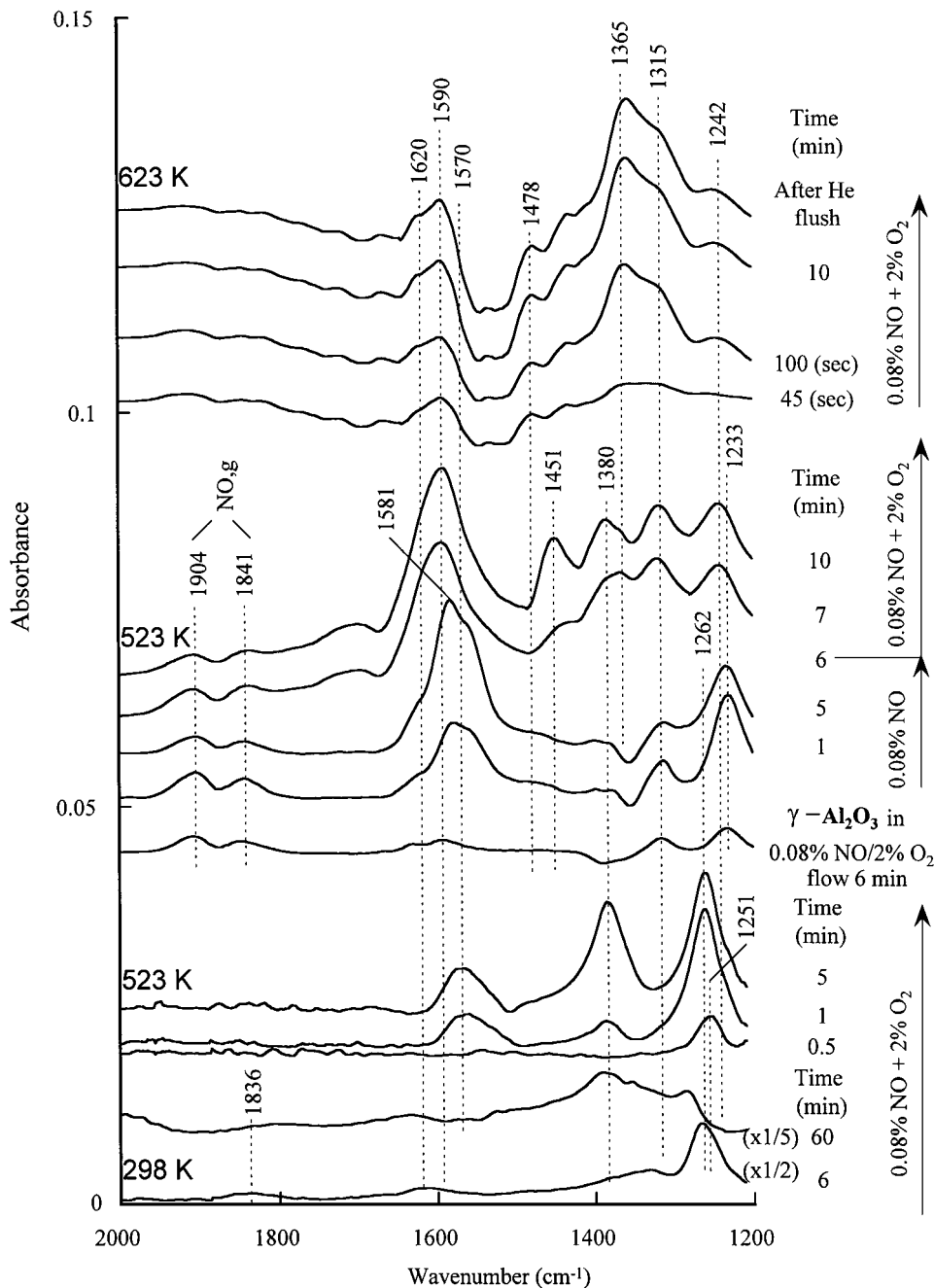


FIG. 5. *In situ* IR spectra produced from (a) flow of 0.08% NO + 2% O₂ + 97.92% He at 523 K, (b) flow of 0.08% NO followed by 2% O₂ addition at 523 K, and (c) flow of 0.08% NO + 2% O₂ + 97.92% He at 623 K over CuO/Al₂O₃.

1233 cm⁻¹. Addition of 2% O₂ to a 0.08% NO flow at 523 K resulted in (i) the formation of monodentate nitrate Cu²⁺-O-N<O at 1451 cm⁻¹ and (NO₃⁻)₂ at 1380 cm⁻¹ and (ii) the shift in wavenumber of Cu²⁺-<O>N-O from 1570 to 1590 cm⁻¹ and that of Cu²⁺-<O>N from 1233 to 1242 cm⁻¹. Formation of (NO₃⁻)₂ and Cu²⁺-O-N<O and an increase in the intensity of Cu²⁺-<O>N-O after O₂ addition suggests the successive oxidation of Cu²⁺-<O>N and Cu²⁺-O-N=O to the various forms of adsorbed nitrates.

The most interesting feature for 0.08% NO/2% O₂ coadsorption on CuO/Al₂O₃ at 623 K is the rapid formation of dominant (NO₃⁻)₂ centered at 1365 cm⁻¹. High temperature is responsible for the low intensity of Cu²⁺-<O>N as well as its wavenumber shift at 623 K. This is further confirmed by the absence of Cu²⁺-<O>N for NO/O₂ coadsorption at 723 K. The absence of gaseous NO₂ formation over CuO/Al₂O₃ indicated that these adsorbed nitrates and nitro groups are formed from the reaction of NO and O₂ on

CuO without a gaseous NO_2 intermediate. The formation of $\text{Cu}^{2+} \langle \text{O} \rangle \text{N}$ and $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$ from NO/O_2 adsorption is thermodynamically favorable (53). The contribution of Al_2O_3 to adsorbate formation on $\text{CuO}/\text{Al}_2\text{O}_3$ was not significant as evidenced by low intensities of $\text{Al}^{3+} \langle \text{O} \rangle \text{N}$ at 1233 cm^{-1} , $\text{Al}^{3+} \text{-O-N=O}$ at 1315 cm^{-1} , $\text{Al}^{3+} \text{-O} \langle \text{O} \rangle \text{N-O}$ at 1630 cm^{-1} , and $\text{Al}^{3+} \langle \text{O} \rangle \text{N-O}$ at 1590 cm^{-1} in Fig. 5. The intensities of these adsorbates are less than 5% of those on $\text{CuO}/\text{Al}_2\text{O}_3$. Therefore, Cu sites are responsible for the formation of $\text{Cu}^{2+}(\text{NO}_3^-)_2$ from flowing $0.08\% \text{ NO} + 2\% \text{ O}_2 + 97.92\% \text{ He}$ over $\text{CuO}/\text{Al}_2\text{O}_3$.

Adsorption of NO_2/O_2 , and NO_2 on $\text{CuO}/\text{Al}_2\text{O}_3$

Figure 6 compares the IR spectra of adsorbates produced from NO_2 and from NO_2/O_2 adsorption on $\text{CuO}/\text{Al}_2\text{O}_3$ at 523 K. Initial exposure of $\text{CuO}/\text{Al}_2\text{O}_3$ to $0.08\% \text{ NO}_2 + 2\% \text{ O}_2 + 97.92\% \text{ He}$ at 523 K produced $\text{Cu}^{2+}(\text{NO}_3^-)_2$ at 1380 cm^{-1} first, then $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$ at 1590 and 1561 cm^{-1} , $\text{Cu}^{2+} \text{-O} \langle \text{O} \rangle \text{N-O}$ at 1620 cm^{-1} , and $\text{Cu}^{2+} \langle \text{O} \rangle \text{N}$ centered at 1262 cm^{-1} . NO_2 adsorption alone cannot produce $\text{Cu}^{2+}(\text{NO}_3^-)_2$ at 1380 cm^{-1} ; however, it produced primarily $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$. The simultaneous presence of

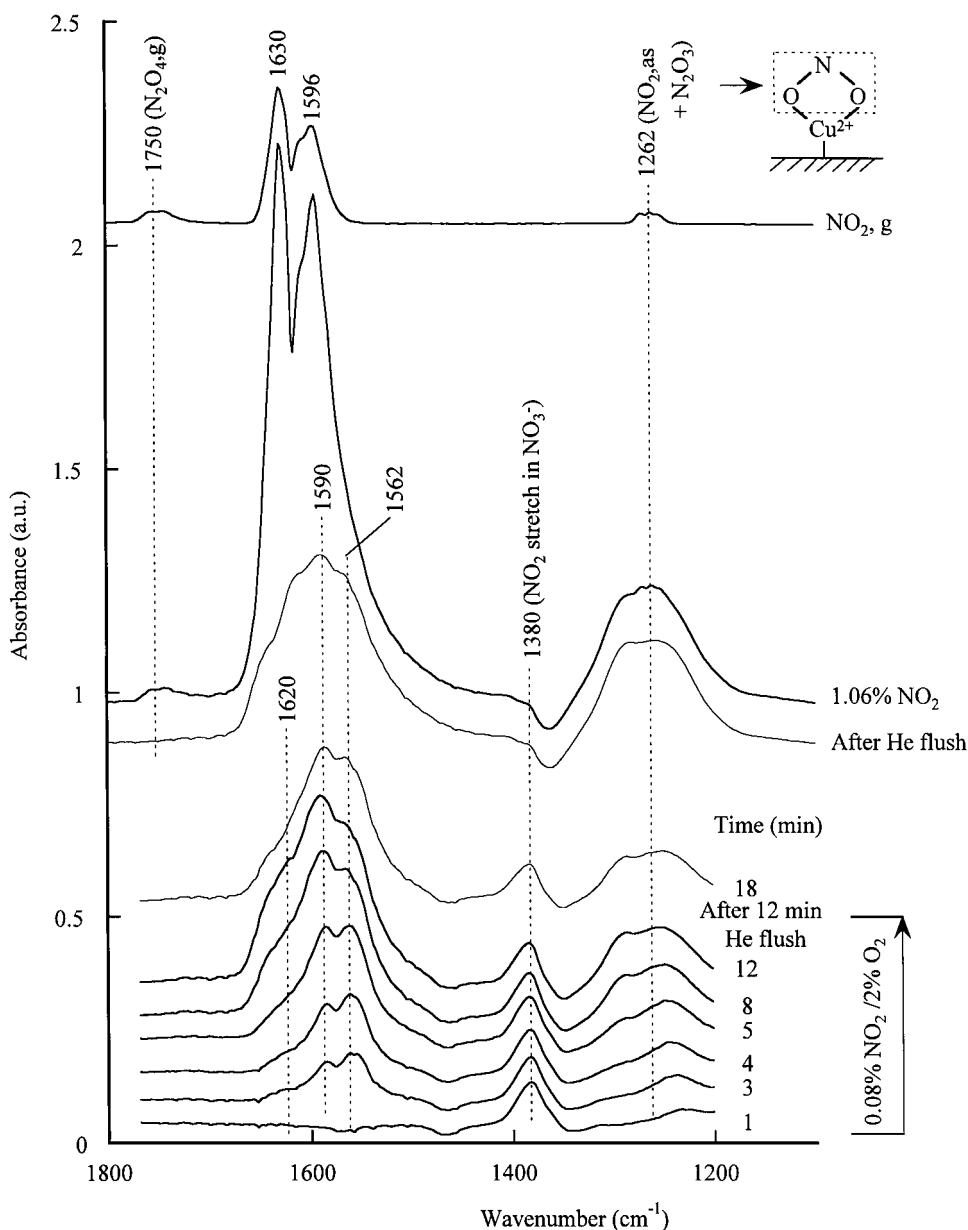


FIG. 6. *In situ* IR spectra of adsorbates produced from flow of $1.06\% \text{ NO}_2$ and from flow of $0.08\% \text{ NO}_2 + 2\% \text{ O}_2 + 97.92\% \text{ He}$ over $\text{CuO}/\text{Al}_2\text{O}_3$ at 523 K for 12 min (thin solid lines were taken after He flush).

O₂ and NO₂ is required to produce Cu²⁺(NO₃⁻)₂ at 1380 cm⁻¹. This observation suggested that O₂ is necessary for Cu²⁺(NO₃⁻)₂ formation. The IR intensity of the band at 1262 cm⁻¹ for NO₂ as well as NO₂/O₂ adsorption was stronger than that for NO/O₂ adsorption. This band can be assigned to the overlap component of Cu²⁺<O>N and adsorbed N₂O₃ (16). At 523 K, NO₂/O₂ adsorption produced a dominant Cu²⁺<O>N-O band while the NO/O₂ adsorption produced an intense Cu²⁺(NO₃⁻)₂ band.

Pulsing C₃H₆ into Steady-State NO/O₂ Flow and Steady-State SCR Reaction of NO/O₂/C₃H₆ on CuO/Al₂O₃

Figure 7 shows the MS profiles and *in situ* IR spectra taken while three consecutive 1-cm³ C₃H₆ pulses were pulsed into the steady-state 0.08% NO + 2% O₂ + 97.92% He flow at 723 K. Pulsing C₃H₆ decreased the NO and O₂ MS intensity (i.e., concentration) and increased the N₂,

CO₂, N₂O, H₂O, and NO₂ concentration. The MS profile of C₃H₆ led those of N₂, CO₂, N₂O, H₂O, and NO₂, consistent with the Langmuir-Hinshelwood mechanism (i.e., reactant adsorption followed by surface reaction and product desorption). Pulsing C₃H₆ also decreased the IR intensity of adsorbed Cu²⁺(NO₃⁻)₂ at 1365 cm⁻¹, indicating that this species may be the active adsorbate responsible for product formation. Gaseous CO₂ at 2358 and 2312 cm⁻¹ emerged as one of the products. Observation of =C-H and C-H bands around 3100–2900 cm⁻¹ was attributed to the incomplete consumption of C₃H₆. The band at 1561 cm⁻¹ was attributed to NO₂ asymmetric vibration in C₃H₇-NO₂ (30, 31, 33, 34, 54, 55). The IR intensity of adsorbed Cu²⁺(NO₃⁻)₂ reached the minimum at 65 s, when NO and O₂ approached the minimum concentration.

Figure 8a shows that exposure of CuO/Al₂O₃ to a 0.08% NO + 2% O₂ + 0.2% C₃H₆ + 97.72% He flow at 523 K produced an organic nitro compound (C₃H₇-NO₂) at 1593 and

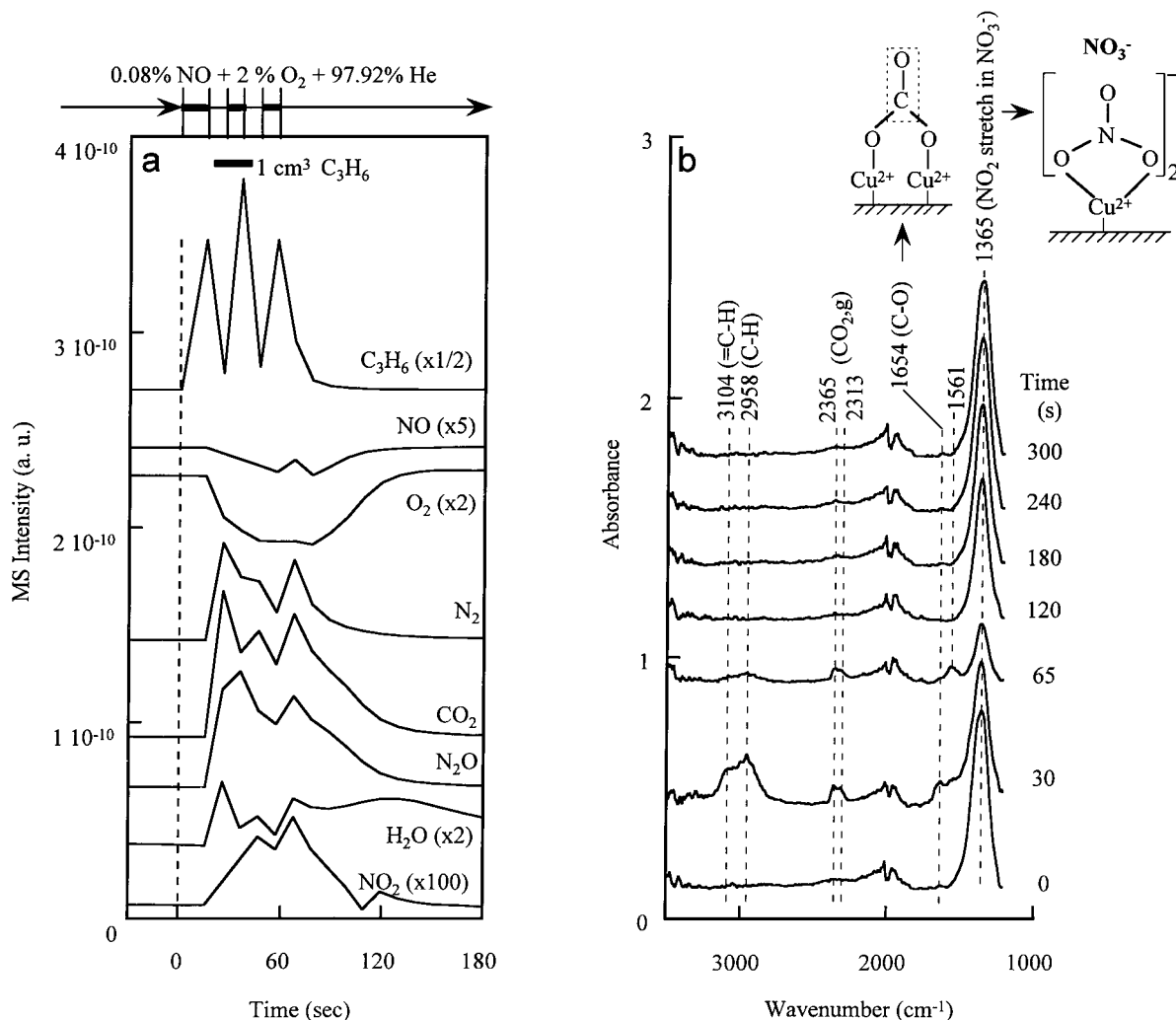


FIG. 7. (a) MS profiles and (b) *in situ* IR spectra taken during pulsing of three consecutive 1-cm³ pulses of C₃H₆ into the steady-state flow of 0.08% NO + 2% O₂ + 97.92% He over CuO/Al₂O₃ at 723 K.

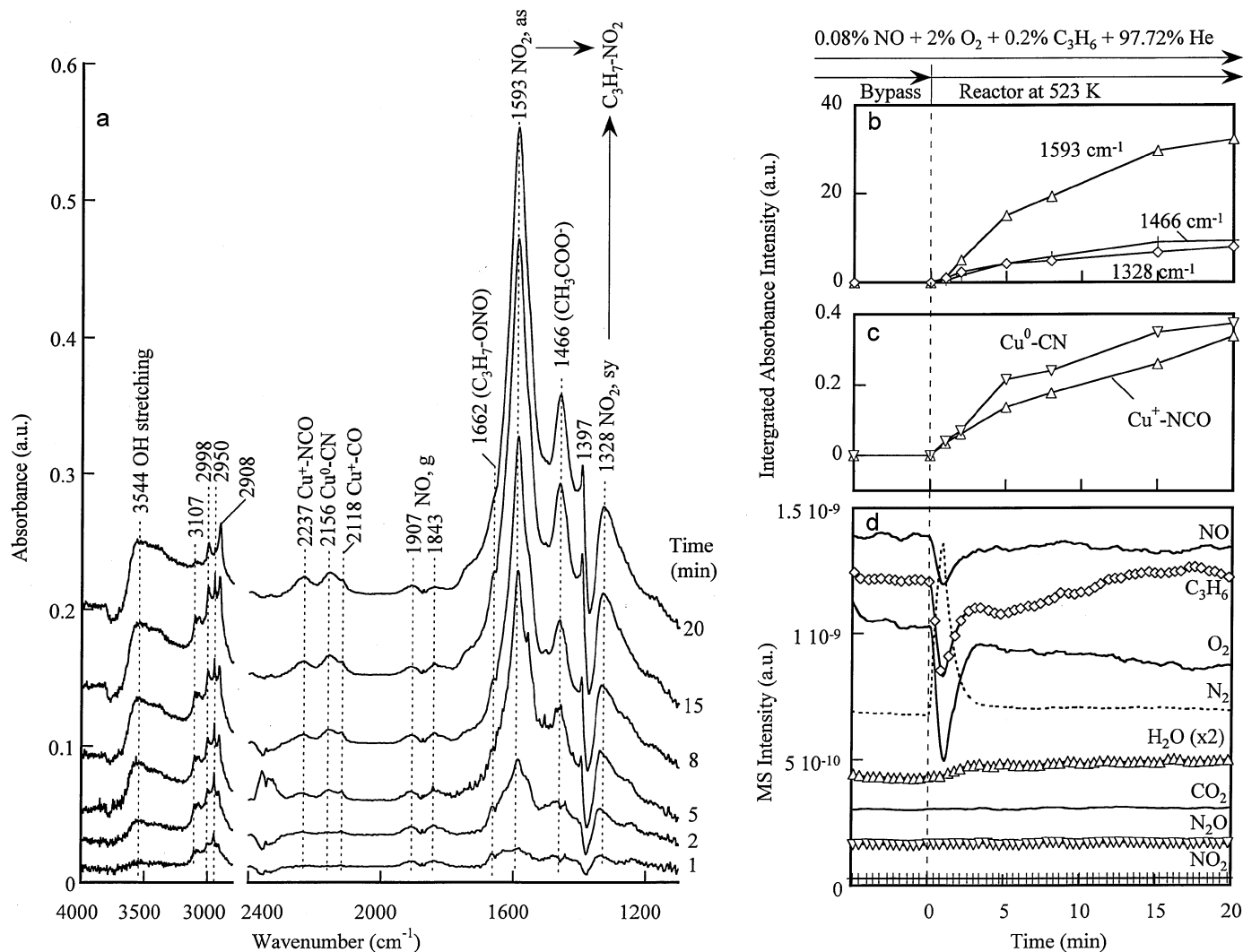


FIG. 8. (a) *In situ* IR spectra of adsorbates. (b) and (c) Integrated absorbance intensity as a function of time obtained from $\bar{A}_{1593} = \int_{1510}^{1780} A(\nu) d\nu$, $\bar{A}_{1466} = \int_{1410}^{1490} A(\nu) d\nu$, $\bar{A}_{1328} = \int_{1200}^{1370} A(\nu) d\nu$, $\bar{A}_{2156} = \int_{2124}^{2190} A(\nu) d\nu$, and $\bar{A}_{2237} = \int_{2200}^{2280} A(\nu) d\nu$, where A_i is the integrated absorbance intensity for species i . (d) MS profiles during switching the flow of 0.08% NO + 2% O₂ + 0.2% C₃H₆ + 97.72% He from bypass into the reactor at 523 K. (H₂O MS profile was enlarged by multiplying by 2.)

1328 cm⁻¹ (30, 31, 33, 34, 54, 55), an organic nitrito compound (C₃H₇-ONO) at 1662 cm⁻¹ (30, 31, 33, 34, 54, 55), an CH₃COO⁻ at 1593 and 1466 cm⁻¹ (35, 36, 54–56), Cu⁺-CO at 2118 cm⁻¹ (25, 28), Cu⁰-CN at 2156 cm⁻¹ (28, 40, 41), Cu⁺-NCO at 2237 cm⁻¹ (28, 35, 57), the OH stretching band at around 3544 cm⁻¹, and C–H asymmetric stretching bands at 3107, 2998, 2950, and 2908 cm⁻¹ (54, 55). The presence of gaseous NO indicated that NO was not reduced/oxidized completely. Absorbance intensity versus time profiles in Figs. 8b and 8c showed that initial formation rate of C₃H₇-NO₂ and CH₃COO⁻ was greater than that of Cu⁰-CN and Cu⁺-NCO. MS analysis of reaction products in Fig. 8d shows that initial exposure of CuO/Al₂O₃ to a NO/O₂/C₃H₆ flow caused a high overshoot in N₂ formation, corresponding to the decrease of NO, C₃H₆, and O₂

concentrations. The H₂O formation profile was enlarged by multiplying by 2 in Fig. 8d.

Table 1 gives the steady-state NO, C₃H₆, and O₂ conversion and N₂ selectivity results at different temperatures and reaction times. Increasing the temperature increased the NO, C₃H₆, and O₂ conversion. N₂ selectivity increased slightly with increasing temperature from 95% to 97%. Our Cu/Al₂O₃ shows activity similar to those reported but with a difference in N₂ yield (27–29).

Figure 9 shows the IR spectra taken during steady-state SCR reaction on Cu/Al₂O₃. Reaction conditions and selectivity results are listed in Table 1. Increasing the temperature caused the intensities of C₃H₇-NO₂, CH₃COO⁻, and gaseous CO₂ to increase. To delineate the change in the contour of the IR bands in the 1350–1700 cm⁻¹ region, the

TABLE 1

Reactant Conversion and N₂ Selectivity during Steady-State 0.08% NO + 6.67% O₂ + 0.2% C₃H₆ + 93.05% He Flow on CuO/Al₂O₃ at Various Temperatures

Temperature (K) and time on stream (min)	0.08% NO + 2% O ₂ + 0.2% C ₃ H ₆ + 97.72% He				
	Conversion (%)			Conversion of NO to N ₂ (%) ^a	N ₂ selectivity (%) ^b
	NO	C ₃ H ₆	O ₂		
523, 10	26.9	30.3	19.3	25.9	96.5
623, 15	35.7	35.0	21.6	34.2	95.7
673, 10	87.6	22.5	32.9	84.5	96.5
698, 10	90.4	29.4	33.8	88.0	97.4
723, 20	96.4	99.0	37.3	94.1	97.6
773, 25	100	100	39.1	97.3	97.3

^a Conversion of NO to N₂ (%) = 2(mol N₂)/mol NO_{in} × 100.

^b N₂ selectivity (%) = 2(mol N₂)/(mol NO_{in} - mol NO_{out}) × 100.

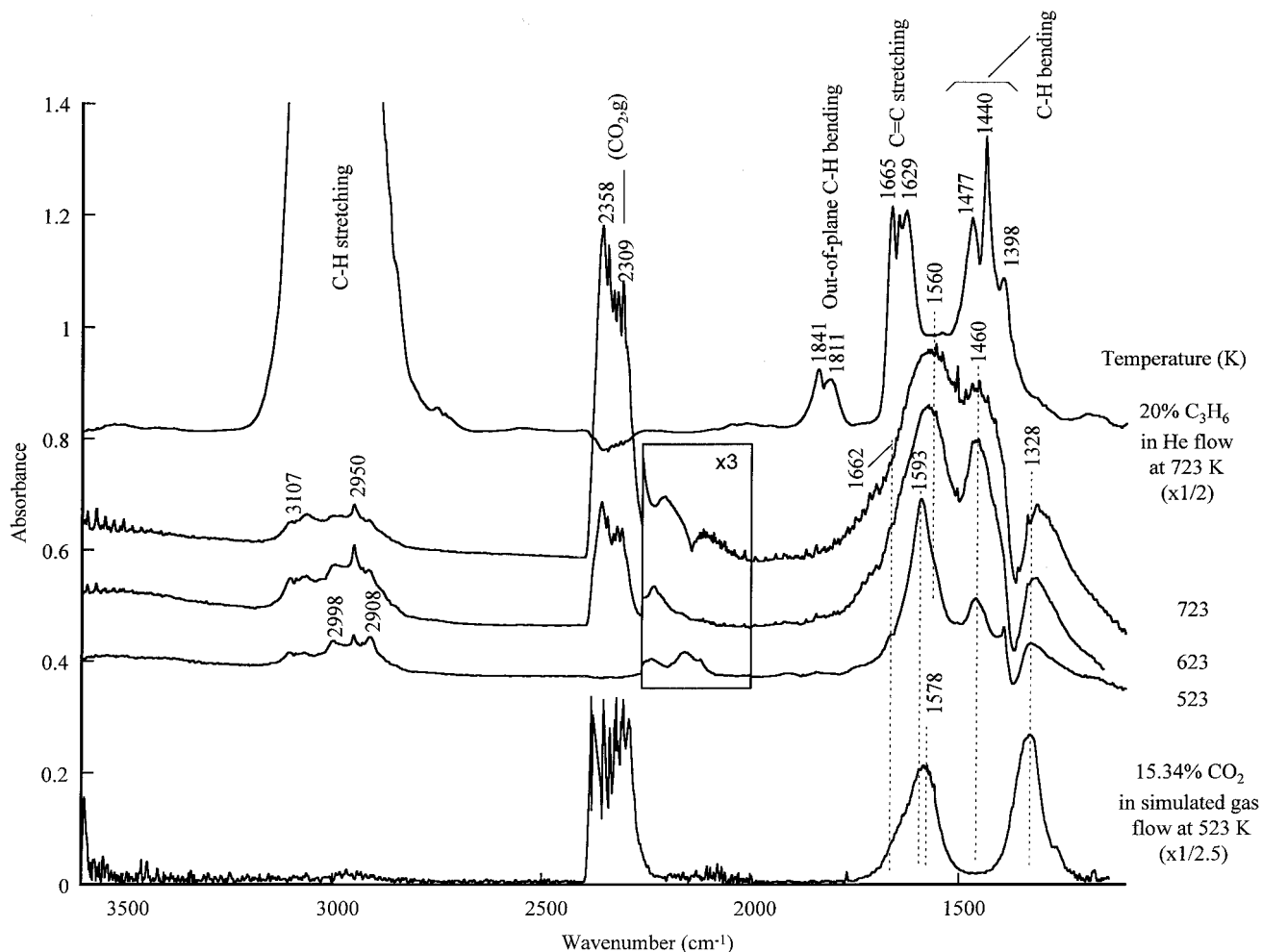


FIG. 9. Steady-state *in situ* IR spectra of adsorbates produced from flow of 0.08% NO + 2% O₂ + 0.2% C₃H₆ + 97.72% He over CuO/Al₂O₃ at various temperatures.

catalyst was exposed to C_3H_6 and automobile exhaust simulated gas (15.34% CO_2 , 0.7765% CO , 0.5392% O_2 , 0.2673% H_2 , and 0.0865% C_3H_8 with He balance), respectively. Comparison of the IR spectra of adsorbates from C_3H_6 to that of $NO/O_2/C_3H_6$ adsorption on CuO/Al_2O_3 indicated that 1328, 1466, and 1593 cm^{-1} bands, attributed to $C_3H_7NO_2$ and CH_3COO^- , cannot be formed from C_3H_6 adsorption alone. CO_2 adsorption from simulated gas on CuO/Al_2O_3 produced chelating carbonate ($Cu^{2+}<O_2>C-O$) and monodentate carbonate ($Cu^{2+}-O-C<O_2>$) at 1578 and 1328 cm^{-1} , respectively (48). The ratio of IR intensity of the band at 1578 cm^{-1} to that of the band at 1328 cm^{-1} was 0.8 for carbonate; however, the ratio was 5.2 for $NO/O_2/C_3H_6$ reaction on CuO/Al_2O_3 at 523 K. The broadening of the 1593 and 1328 cm^{-1} bands at 623 and 723 K can be attributed to overlapping of carbonate bands with the $C_3H_7NO_2$ and CH_3COO^- bands. The broadening of these bands is accompanied by strong gaseous CO_2 bands at 723 K, fur-

ther confirming the contribution of carbonates from CO_2 adsorption.

The obvious effects of temperature are (i) the increase in the CH_3COO^- intensity at 1460 cm^{-1} and (ii) the shift in the wavenumber of the band from 1593 to 1560 cm^{-1} . To further unravel the dynamic behavior of $C_3H_7NO_2$ at 1560 and 1314 cm^{-1} and of CH_3COO^- at 1460 cm^{-1} , the C_3H_6 flow was stopped while NO , O_2 , and He flows were kept at steady state and 723 K. Figure 10 shows the variation of *in situ* IR spectra of adsorbates as a function of time after the C_3H_6 flow was stopped at 723 K. Disappearance of C_3H_6 resulted in (i) immediate disappearance of C_3H_6 -related bands and (ii) a gradual decay of $C_3H_7NO_2$ and CH_3COO^- . Upon disappearance of the $C_3H_7NO_2$ and CH_3COOH species, gaseous NO_2 and adsorbed $Cu^{2+}(NO_3^-)_2$ emerged. The appearance of $C_3H_7NO_2$ at 1560 cm^{-1} at 723 K is consistent with that of $C_3H_7NO_2$ at 1561 cm^{-1} during the C_3H_6 pulse in Fig. 7b.

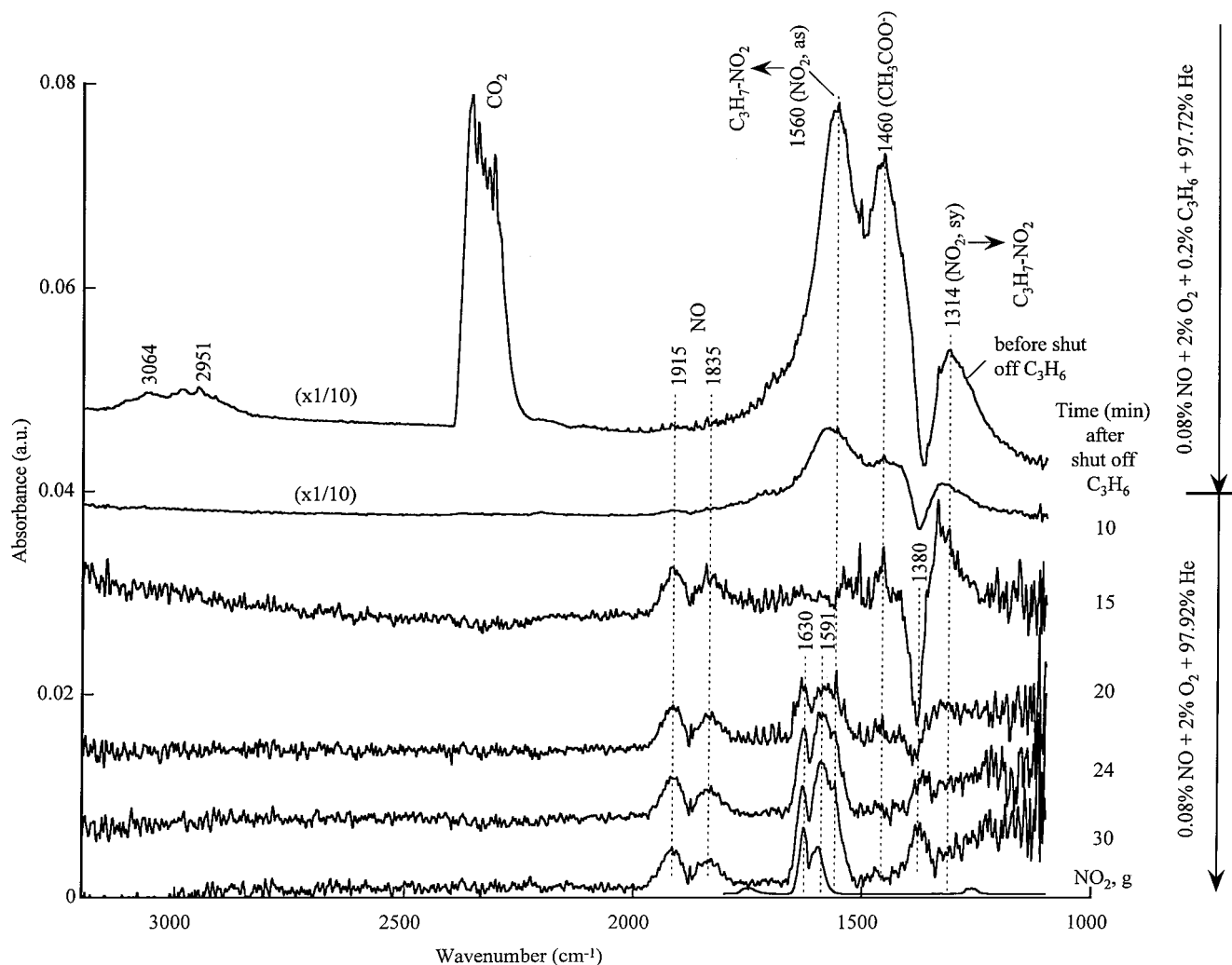


FIG. 10. Variation of *in situ* IR spectra of adsorbates as a function of time after shut-off of C_3H_6 from 0.08% NO + 2% O_2 + 0.2% C_3H_6 + 97.72% He flow over CuO/Al_2O_3 at 723 K.

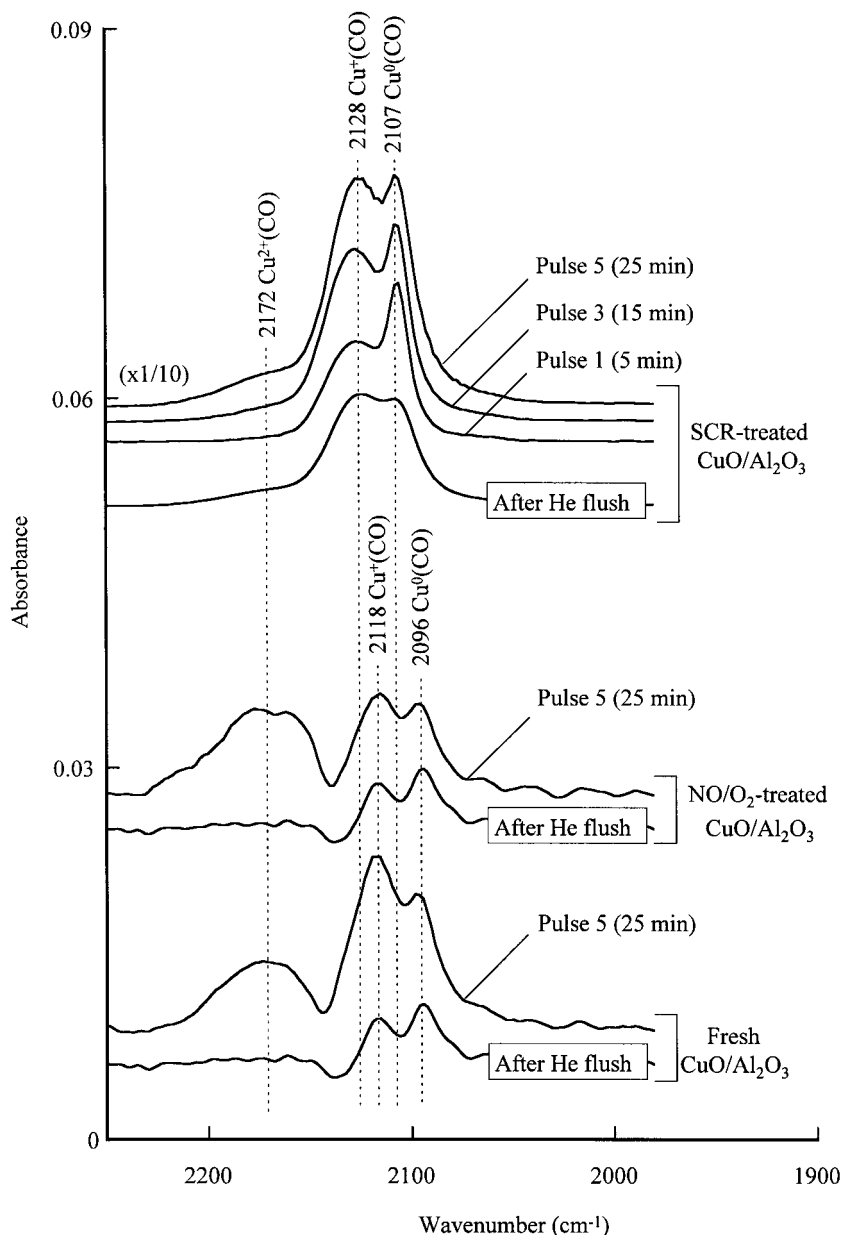


FIG. 11. *In situ* IR spectra taken during exposure of fresh CuO/Al₂O₃, NO/O₂-treated CuO/Al₂O₃, and SCR-treated CuO/Al₂O₃ to CO pulse (top spectrum for each catalyst) and after exposure to He flowing at 75 cm³/min (bottom spectrum for each catalyst) for 5 min at 298 K. Fresh CuO/Al₂O₃ is produced from the thermal decomposition of Cu(NO₃)₂ on Al₂O₃ in He flow; NO/O₂-treated CuO/Al₂O₃ is obtained after NO/O₂, NO₂, NO₂/O₂ desorption and subsequent TPD studies; and SCR-treated CuO/Al₂O₃ is produced after SCR reaction at 773 K.

CO Chemisorption on CuO/Al₂O₃

Pulsing CO on fresh CuO/Al₂O₃ at 298 K produced Cu²⁺(CO) at 2172 cm⁻¹ (25, 28, 37), Cu⁺(CO) at 2118 cm⁻¹, and Cu⁰(CO) at 2096 cm⁻¹ (25), as shown in Fig. 11. Each CO pulse consists of 10 cm³ of 99.994% CO. The IR spectra were collected immediately after the CO pulse. Pulsing CO allows the determination of the amount of CO adsorbed on the catalyst surface. CO preferably adsorbed on Cu⁰ initially

and then on Cu⁺ over SCR-treated CuO/Al₂O₃. Flowing He over adsorbed CO species decreased the IR intensities of all species, consistent with the observations on Cu/Al₂O₃ at 300 K (25). No adsorbed CO was observed on γ -Al₂O₃ under the conditions of this study. Adsorption of CO on α -Al₂O₃ has been reported to give a band at 2150 cm⁻¹ (58). The IR band intensity corresponds to the concentration of adsorbates, also reflecting the number of specific adsorption sites. However, the lack of extinction coefficients for

these various forms of adsorbed CO does not allow the use of these adsorbate intensities to determine the number of Cu^0 , Cu^+ , and Cu^{2+} sites. Qualitatively speaking, exposure of $\text{CuO}/\text{Al}_2\text{O}_3$ to the NO/O_2 flow decreased more Cu^+ than Cu^0 sites and converted a portion of Cu^0/Cu^+ sites to Cu^{2+} sites; the SCR reduced almost all Cu^{2+} sites to Cu^0/Cu^+ sites. Assuming the extinction coefficient for adsorbed CO is independent of its coverage, a significant increase in adsorbate intensity reflects the increase in the number of adsorption sites. The amount of CO adsorbed is determined to be $29.5 \mu\text{mol}$ for the SCR-treated catalyst and $2.5 \mu\text{mol}$ for the fresh $\text{CuO}/\text{Al}_2\text{O}_3$, indicating the SCR not only reduced Cu^{2+} to Cu^+/Cu^0 but also increased the dispersion of Cu^0/Cu^+ species on the Al_2O_3 surface.

DISCUSSION

Formation of Adsorbed NO_x from NO/O_2 and NO_2/O_2

The broad bands in the regions of $1500\text{--}1670 \text{ cm}^{-1}$ and $1200\text{--}1350 \text{ cm}^{-1}$ observed in this study result from overlapping of multiple bands. Although most of these bands cannot be unambiguously assigned, the observation of a singly

symmetric band at 1380 cm^{-1} in Figs. 4, 6, and 7 as well as at 1242 cm^{-1} in Fig. 5 allows assignment of these bands to specific NO_x species. Band assignment here follows the classical works reported by Nakamoto (47) and Davydov (48), previous literature (21–45, 49–52), and the IR spectra of $\text{Cu}(\text{NO}_3)_2$ and $\text{Cu}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}/\text{Al}_2\text{O}_3$ in Fig. 1.

Adsorption studies shown in Fig. 5 demonstrate that NO/O_2 adsorption on $\text{CuO}/\text{Al}_2\text{O}_3$ led to immediate formation of $\text{Cu}^{2+}\langle\text{O}\rangle\text{N}$ and gradual formation of $\text{Cu}^{2+}(\text{NO}_3)_2$ at 523 K; Fig. 6 shows that NO_2/O_2 adsorption led to immediate formation of $\text{Cu}^{2+}(\text{NO}_3)_2$ and gradual formation of $\text{Cu}^{2+}\langle\text{O}\rangle\text{N-O}$, $\text{Cu}^{2+}\langle\text{O}\rangle\text{N-O}$, and $\text{Cu}^{2+}\langle\text{O}\rangle\text{N}$. NO_2 adsorption alone did not lead to the formation of $\text{Cu}^{2+}(\text{NO}_3)_2$; NO_2 adsorption produced only $\text{Cu}^{2+}\langle\text{O}\rangle\text{N-O}$, $\text{Cu}^{2+}\langle\text{O}\rangle\text{N-O}$, and $\text{Cu}^{2+}\langle\text{O}\rangle\text{N}$ species. It is hoped that the adsorbate dynamics will provide insight into the reaction pathways during NO/O_2 adsorption and the SCR of NO_x in the presence of O_2 .

Figure 12 illustrates the pathway for the formation of NO_x species. The thickness of the arrow indicates the rate of each step (e.g., thicker arrow for higher rate). The Cu site which is associated with $(\text{NO}_3)_2$ appears to be in the

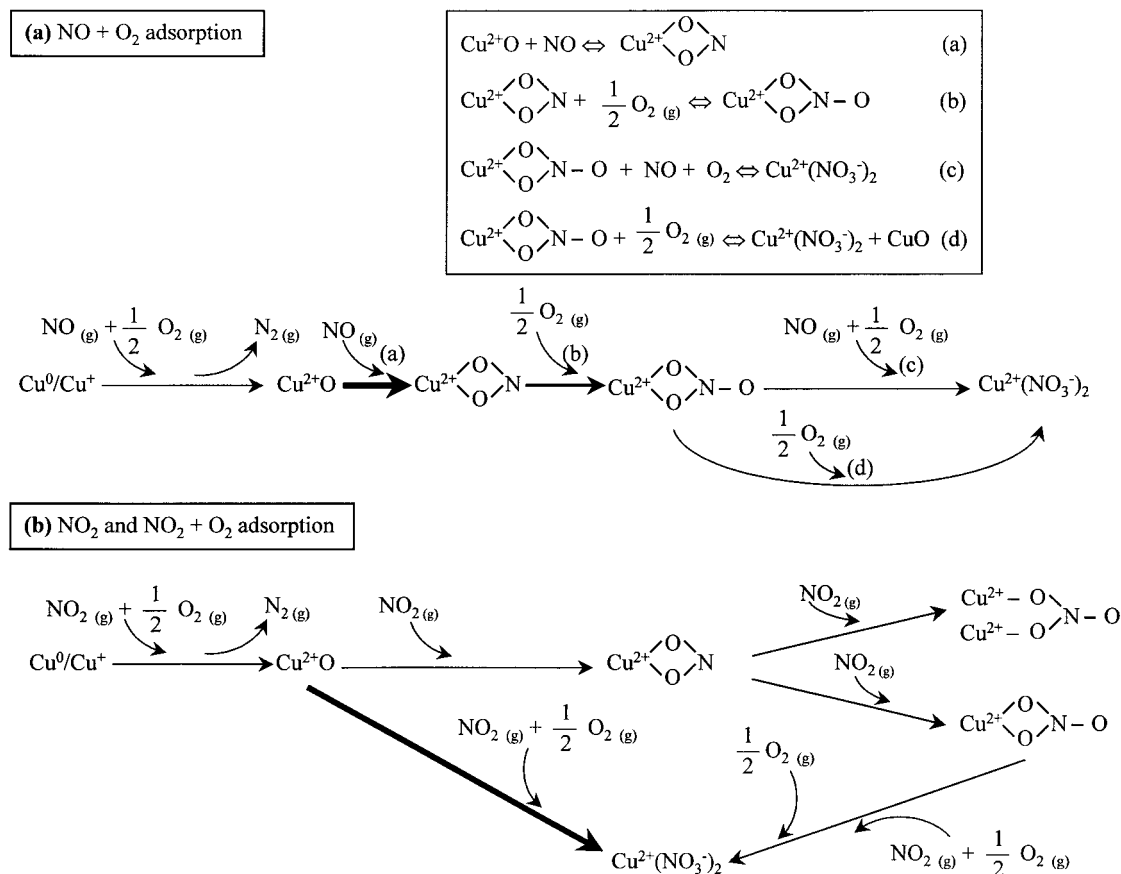


FIG. 12. Proposed pathway for (a) 0.08% $\text{NO} + 2\% \text{O}_2$ adsorption and (b) 1.06% NO_2 and 0.08% $\text{NO}_2 + 2\% \text{O}_2$ adsorption over $\text{CuO}/\text{Al}_2\text{O}_3$.

2+ state since (i) the IR spectrum of these adsorbed (NO₃⁻)₂ species in Figs. 5 and 6 resembles that of Cu²⁺(NO₃⁻)₂ and (ii) NO/O₂ exposure not only produced Cu²⁺(NO₃⁻)₂ but also caused a significant increase in Cu²⁺ sites, as shown in Fig. 11.

Formation of Cu²⁺(NO₃⁻)₂ from NO/O₂ adsorption can be written as a series of well-defined steps, (a), (b), (c), and (d) in Fig. 12. Step (a) is evidenced by the formation of Cu²⁺<O>N from NO adsorption on CuO/Al₂O₃ shown in Fig. 5. Step (b) describes the growth of Cu²⁺<O>N-O upon addition of O₂. Steps (c) and (d) are supported by the observation of (i) rapid growth of Cu²⁺(NO₃⁻)₂ at high temperature (i.e., 623 K) and (ii) conversion of Cu²⁺<O>N-O to Cu²⁺(NO₃⁻)₂ upon increasing the temperature from 523 to 623 K (not shown) (59).

All of the steps involved in the formation of Cu²⁺<O>N-O from NO/O₂, NO₂/O₂, and NO₂ are thermodynamically favorable with a large negative value of Δ*G*^o at 773 K (53). The formation of these adsorbed NO_x species from NO/O₂ rather than from pure NO₂ appears to be related to the nature of the site for adsorption rather than the thermodynamic driving force. The absence of Cu⁺(NO) at tem-

peratures greater than 523 K suggests that Cu⁺ and possibly Cu⁰ sites are oxidized to Cu²⁺ during the NO/O₂ and NO₂/O₂ adsorption processes.

SCR Pathway

IR results of pulsing C₃H₆ and steady-state SCR studies in Figs. 7–10 show that the catalyst surface states and their adsorbates are strongly influenced by reaction environment (i.e., partial pressures of reactants and reaction temperature). Figure 13a illustrates the reaction pathways for the pulse SCR on CuO/Al₂O₃ according to the observed adsorbates and products. The NO/O₂ steady-state flow simulates the exhaust composition of lean burn combustion in which NO and O₂ adsorption on Cu/Al₂O₃ produced Cu²⁺(NO₃⁻)₂. These nitrates adsorbed primarily on Cu²⁺. Each mole of Cu²⁺ on Al₂O₃ adsorbed approximately 0.50 mol of NO at 523 K. Increasing the temperature from 298 to 723 K decreased the amount of NO adsorbed on Cu/Al₂O₃. Pulsing C₃H₆ not only removed (NO₃⁻)₂ adsorbed on Cu²⁺ species but also led to reduction of Cu²⁺ to Cu⁰/Cu⁺ and CO₂ formation. CuO/Al₂O₃ not only serves as a good sorbent for NO/O₂ but also exhibits high selectivity

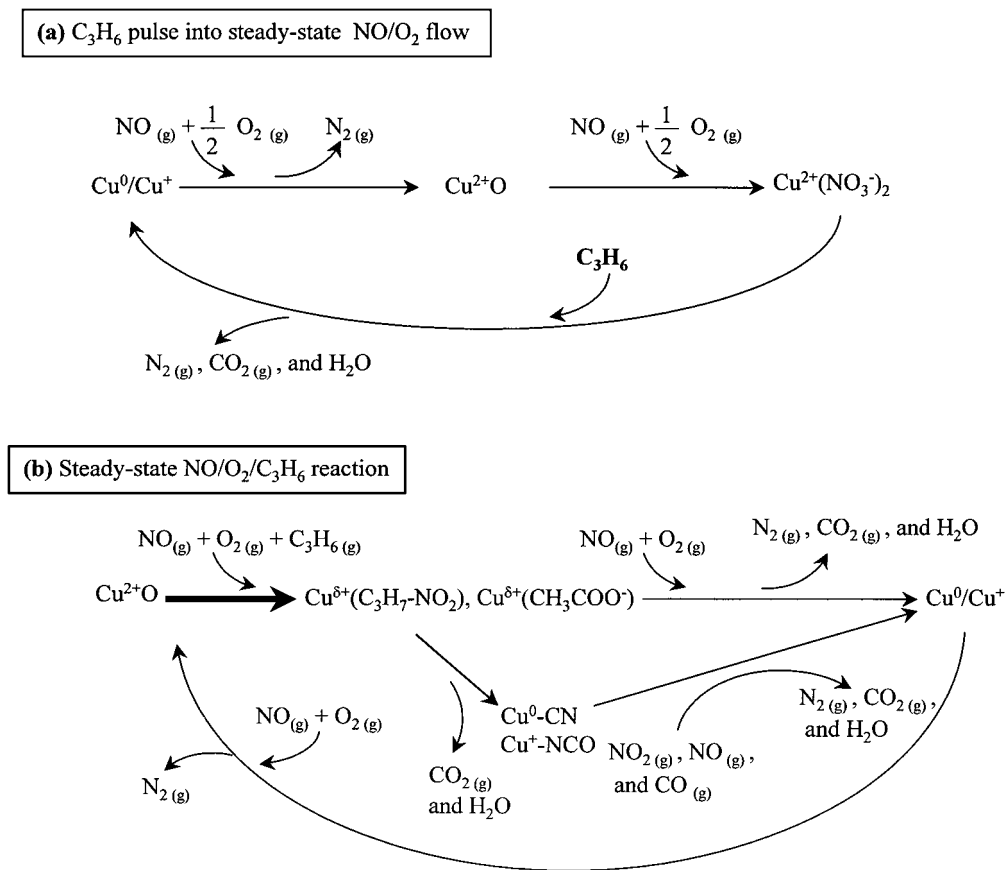


FIG. 13. Proposed pathway for (a) reaction between adsorbed (NO₃⁻)₂ with C₃H₆ pulse and (b) steady-state SCR of NO with C₃H₆ in the presence of O₂ over CuO/Al₂O₃.

for converting $(\text{NO}_3^-)_2$ to N_2 with C_3H_6 . Different forms of nitrates on Al_2O_3 (36) and Rh–Al–MCM-41 (39) have also been recently found to react with C_3H_6 .

The key difference in adsorbates and Cu surface state between pulse and steady-state SCR can be simply attributed to the competitive adsorption of reactants. In the pulse SCR, NO/O_2 oxidizes the Cu in $\text{CuO}/\text{Al}_2\text{O}_3$ to Cu^{2+} , adsorbing $(\text{NO}_3)_2$ prior to the C_3H_6 pulse entering the reactor. In the steady-state SCR in Fig. 13b, C_3H_6 competes over NO/O_2 for adsorption, keeping Cu in either the Cu^0 or Cu^+ state and allowing the formation of $\text{C}_3\text{H}_7\text{-NO}_2$ and CH_3COO^- , as potential intermediates. These intermediates appear to be associated with either Cu^0/Cu^+ or Al_2O_3 surface sites since the catalyst contained fewer Cu^{2+} sites following the SCR as evidenced by the CO adsorption results in Fig. 11.

The proposed scheme in Fig. 13b suggests that adsorbed $\text{C}_3\text{H}_7\text{-NO}_2$ may be further converted to adsorbed $\text{Cu}^0\text{-CN}$ and $\text{Cu}^+\text{-NCO}$ species. The high initial rate of $\text{C}_3\text{H}_7\text{-NO}_2$ formation compared to that of $\text{Cu}^0\text{-CN}$ formation in Figs. 8b and 8c further supports the conclusion that the reaction sequence proceeds via $\text{C}_3\text{H}_7\text{-NO}_2$ and then $\text{Cu}^0\text{-CN}$ and $\text{Cu}^+\text{-NCO}$, since the preceding intermediate has a higher initial rate than the subsequent intermediate in a consecutive reaction (60). The absence of $\text{C}_3\text{H}_7\text{-NO}_2/\text{CH}_3\text{COOH}$ in the gas phase and the immediate disappearance of these species following termination of the C_3H_6 flow suggest that these species are unstable and may be reaction intermediates. No definite evidence is available to either support or dispute $\text{C}_3\text{H}_5\text{-NO}_2/\text{CH}_3\text{COO}^-$ as active intermediates for the reaction. Although R-NO_2 , R-ONO , and CH_3COO^- produced from the $\text{NO}/\text{O}_2/\text{C}_3\text{H}_6$ flow have been found to produce N_2 and CO_2 during their exposure to NO/O_2 (3, 30, 33, 34, 36, 61, 62), their role in the reaction mechanism needs to be further verified by using an isotopic tracing technique under reaction conditions where all the reactants and products are present.

CONCLUSIONS

Infrared spectroscopy coupled with mass spectroscopy allows the determination of the dynamic behavior of adsorbate and product formation during NO/O_2 adsorption, decomposition, and $\text{NO}/\text{O}_2/\text{C}_3\text{H}_6$ reaction. Adsorption studies from 298 to 723 K show that adsorption of NO/O_2 , NO_2/O_2 , and NO_2 produced various adsorbed nitrates on $\text{CuO}/\text{Al}_2\text{O}_3$. NO/O_2 adsorption led to immediate formation of $\text{Cu}^{2+} \langle \text{O} \rangle \text{N}$ and gradual formation of $\text{Cu}^{2+}(\text{NO}_3)_2$; NO_2/O_2 adsorption led to rapid formation of $\text{Cu}^{2+}(\text{NO}_3)_2$ and gradual formation of $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$, $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$, and $\text{Cu}^{2+} \langle \text{O} \rangle \text{N}$; NO_2 adsorption produced only $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$, $\text{Cu}^{2+} \langle \text{O} \rangle \text{N-O}$, and $\text{Cu}^{2+} \langle \text{O} \rangle \text{N}$ species. TPD studies show that adsorbed $(\text{NO}_3^-)_2$, the dominant nitrate, decomposed to N_2 , N_2O , and NO at 644 K.

Steady-state $\text{NO}/\text{O}_2/\text{C}_3\text{H}_6$ reaction on $\text{CuO}/\text{Al}_2\text{O}_3$ produced adsorbed $\text{C}_3\text{H}_7\text{-NO}_2$, $\text{C}_3\text{H}_5\text{-ONO}$, CH_3COO^- , $\text{Cu}^+\text{-NCO}$, $\text{Cu}^0\text{-CN}$, and $\text{Cu}^+\text{-CO}$ species, and N_2 , CO_2 , and H_2O as products. The dynamic behavior of adsorbates under transient conditions suggests that the steady-state SCR proceeds via adsorbed $\text{C}_3\text{H}_7\text{-NO}_2$, $\text{Cu}^0\text{-CN}$, and $\text{Cu}^+\text{-NCO}$ intermediates on Cu^0/Cu^+ sites. Transient formation of N_2 from NO/O_2 adsorption on the fresh $\text{Cu}/\text{Al}_2\text{O}_3$ catalyst at 523 K was attributed to N–N bond formation on Cu^0 site from decomposed nitrate species. Production of N_2 is accompanied by the formation of a Cu^{2+} site, adsorbing NO and O_2 as $(\text{NO}_3^-)_2$. Pulsing C_3H_6 into NO/O_2 over $(\text{NO}_3^-)_2$ on the Cu^{2+} site not only reduced Cu^{2+} to Cu^+/Cu^0 but also converted $(\text{NO}_3^-)_2$ to N_2 and N_2O . Varying the reactant concentration changes the adsorbate concentration and shifts the reaction pathways for SCR.

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